

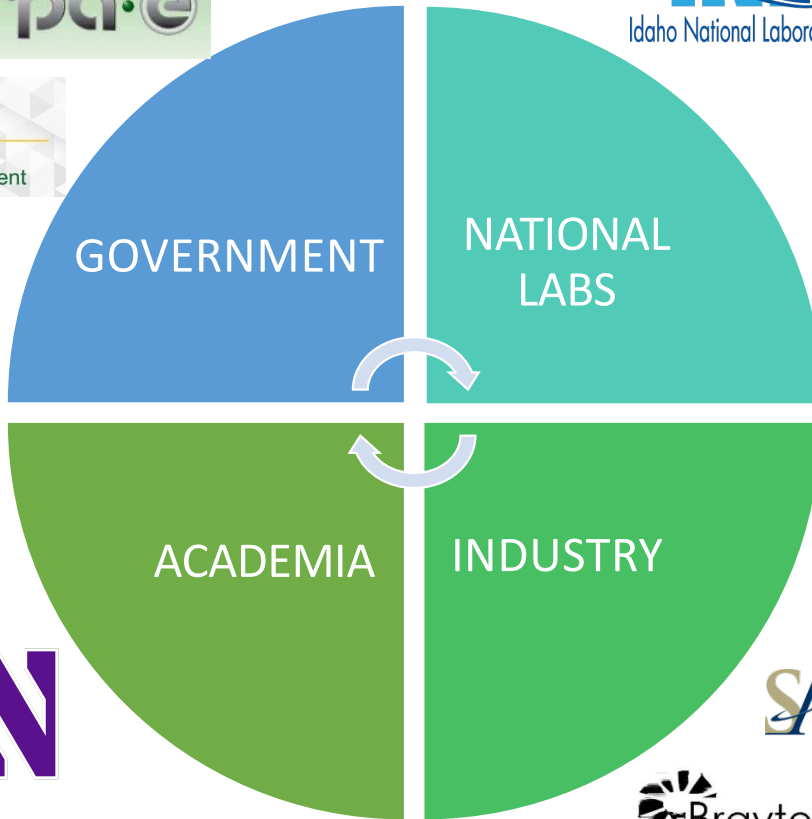
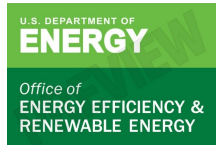
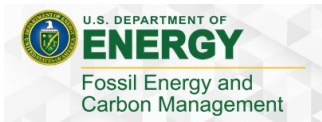
# Cost Analysis of Syngas Production with Nexceris' Co-Electrolysis Technology

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Senior Program Manager, Solid Oxide Business Unit



# Acknowledgements

Our Partners, Collaborators & Sponsors




Pradeep Sharma,  
Lisa Tarr  
Sameer Parvthikar

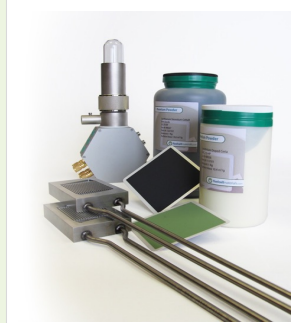




## Where energy meets environment

### Materials

Solid oxide cells and energy storage



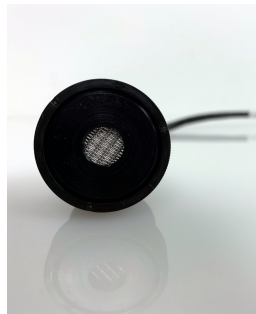
### Solid Oxide Stacks

Stationary and military



### Sensors

Transportation and energy markets



### Catalysts

H<sub>2</sub> and chemicals production



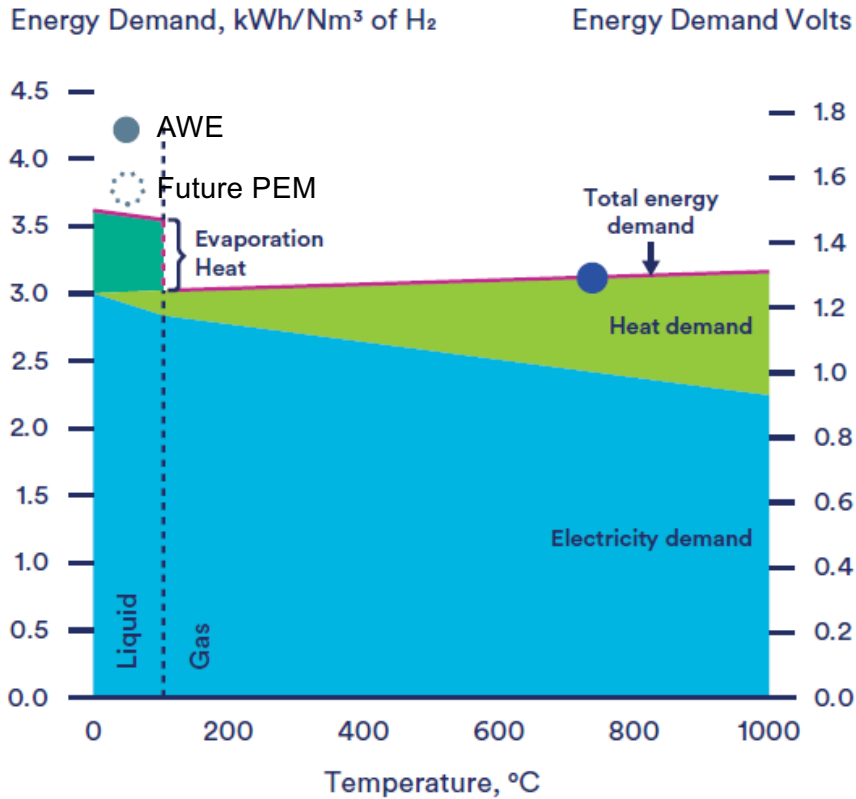
### Protective Coatings

Solid oxide and high temperature





## Thermodynamic favorability



	SOEC	PEM	AWE
electrolyte	ceramic	polymer	KOH
System efficiency (KWh/Kg. H <sub>2</sub> )	38-48	50-83	50-78
Degradation (%/1000h)	0.5	0.25	0.13
Stack life (hours)	50k	50-90k	60-100k
Operating temp (°C)	600-800	50-80	70-90
Co-electrolysis (syngas)	yes	no	no



# Nexceris Solid Oxide Cell (SOC) Technologies

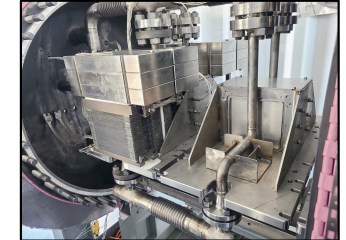
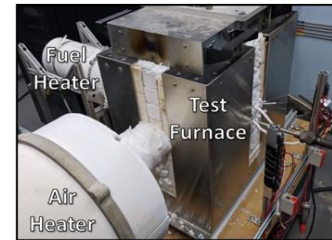
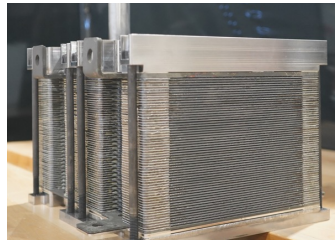
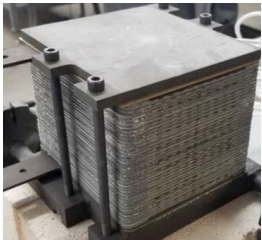
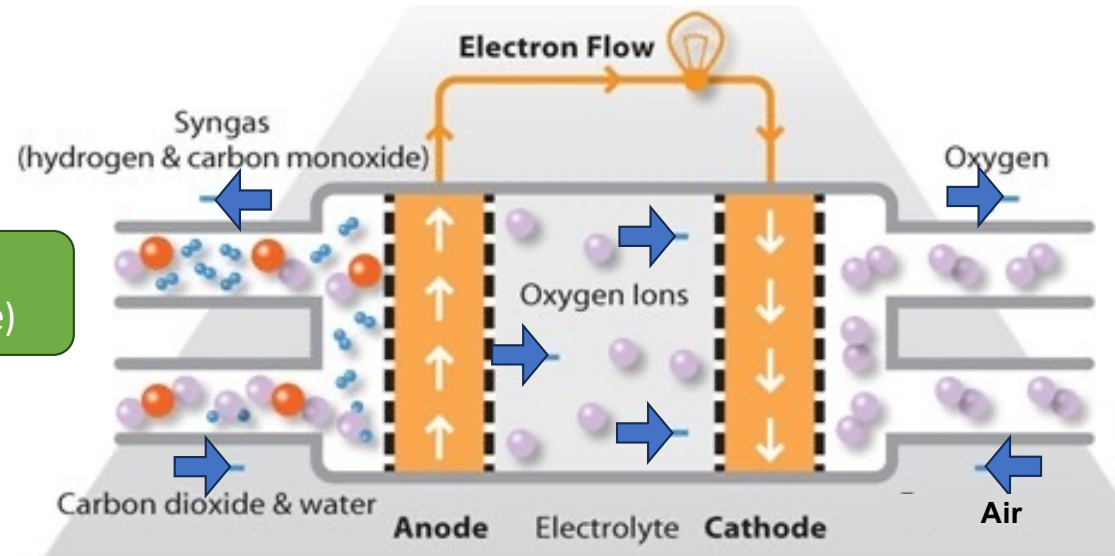
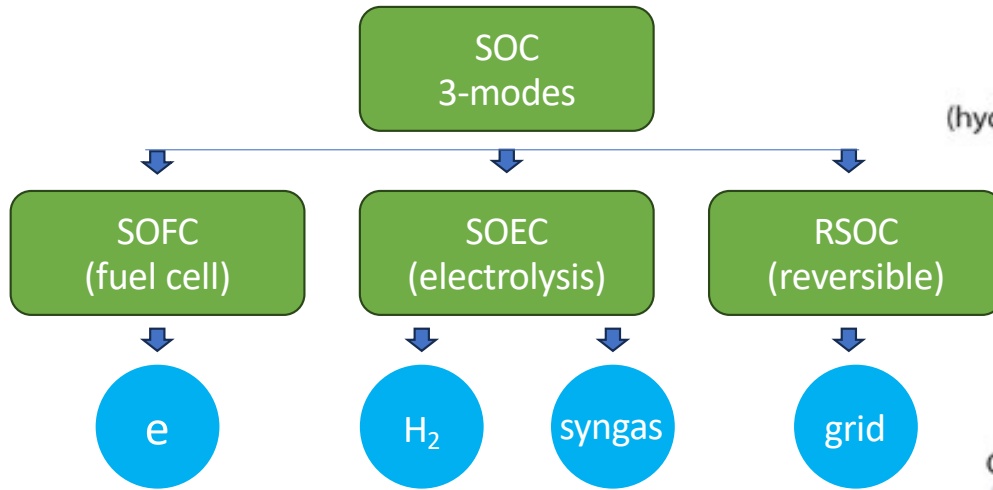
Intro

SOFC

SOEC

Re-SOC

X

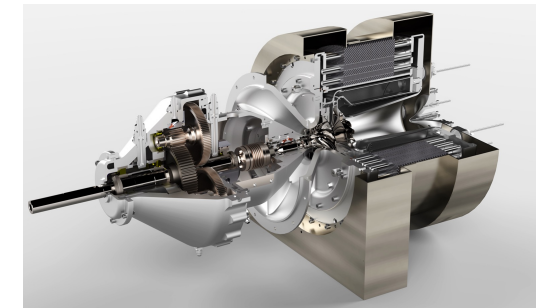
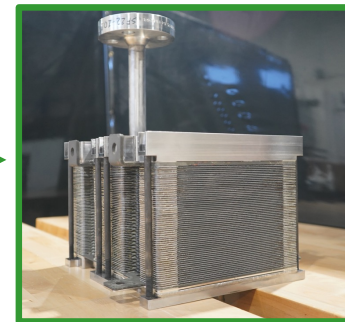
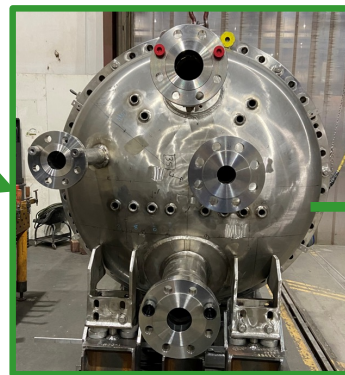
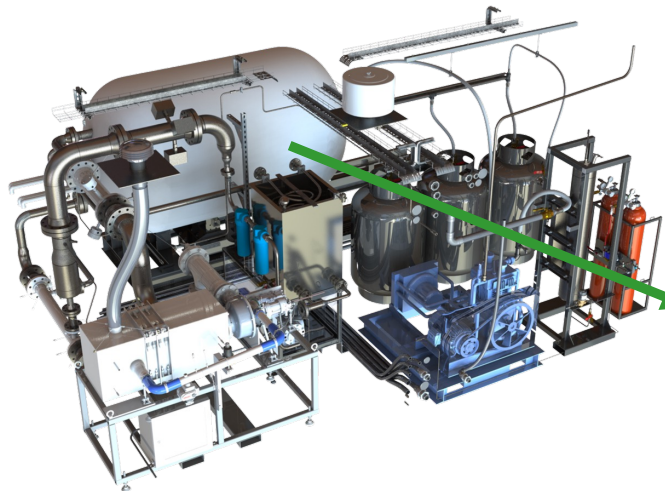
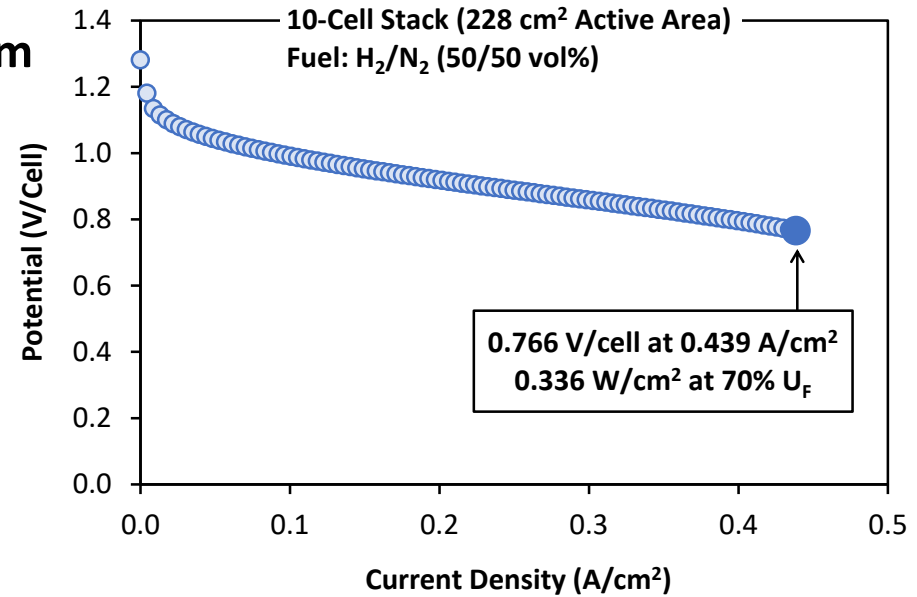


# SOFC – Turbine Integration Project



## High Efficiency SOFC/Turbine Hybrid Power System

- 50 kWe power to operate on natural gas
- Unutilized fuel expands in gas turbine
- Target LHV efficiency is 70%
- High pressure stack operation at 2-3 bar
- System under construction, demo next month.

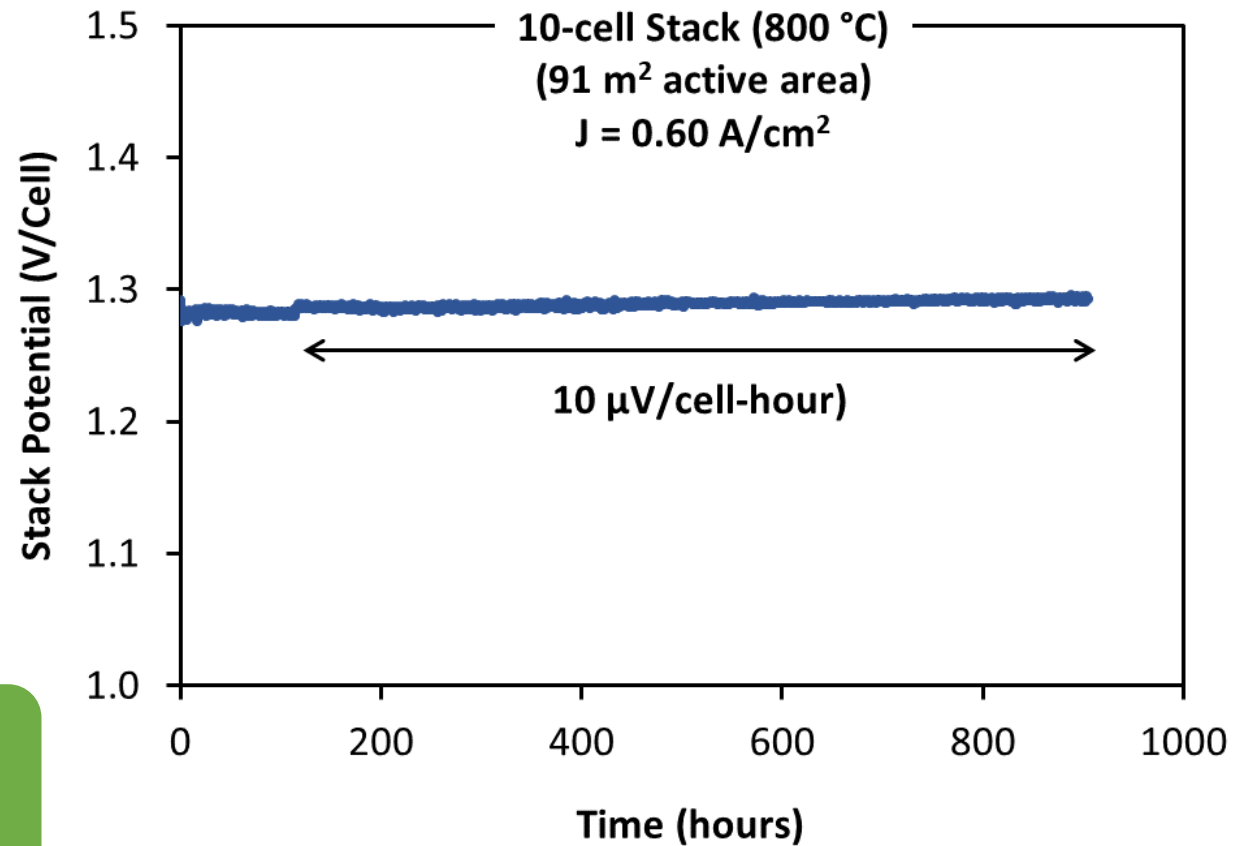




## Long term durability is key

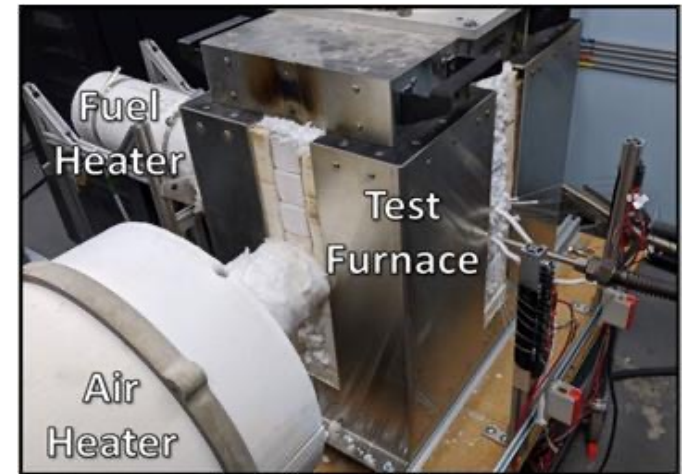
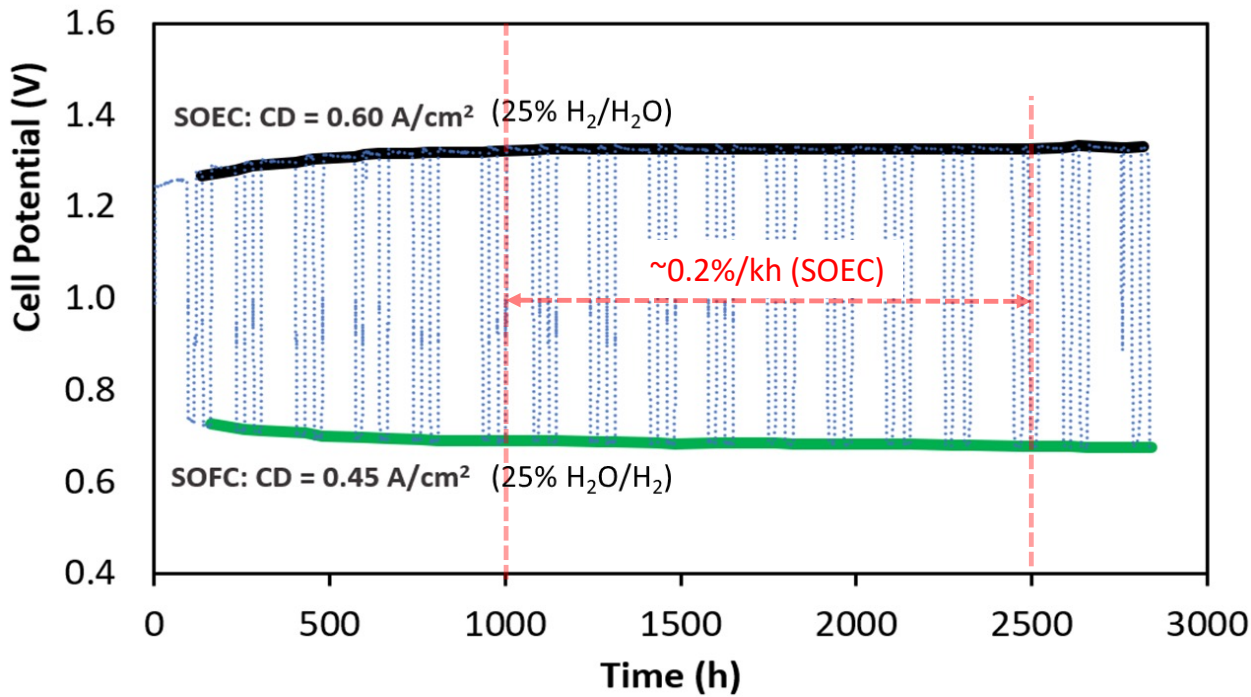
- Our current long term stack degradation target is 10  $\mu\text{V}/\text{hour}$  (achieved).
- Even better durability expected as technology matures.
- Long duration testing is required (and is ongoing).

Nexceris won \$60 million cooperative agreement grant from DOE to scale up SOEC production.





## Stack level performance and durability





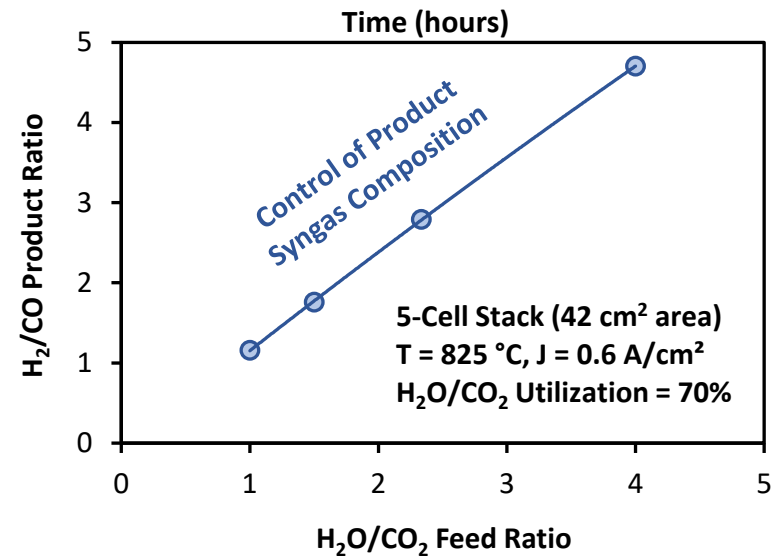
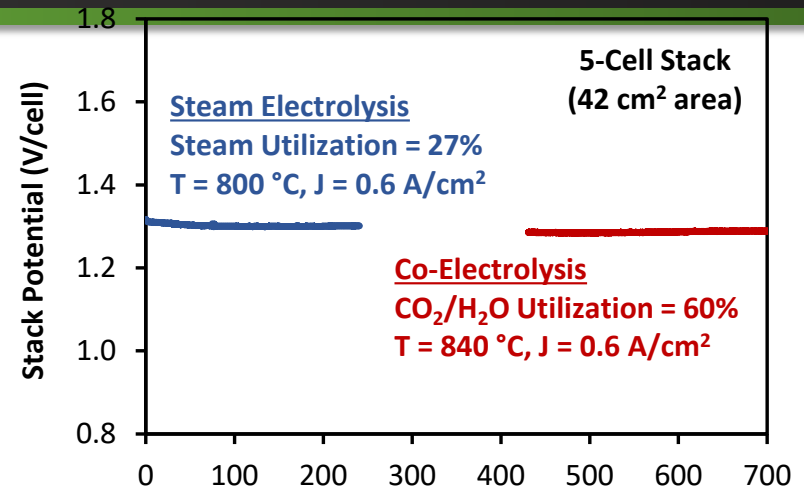


# Power-to-X by Co-electrolysis



## Path to Carbon-neutral production of fuels

- Co-electrolysis of steam and CO<sub>2</sub> into syngas, further converted into value added chemicals / fuels
- Nexceris looking into this technology to potentially combine it with our Fischer-Tropsch catalyst technology that we have been developing
- Our stacks can operate stably in the co-electrolysis and it is possible modulate the syngas composition by controlling the feed input.



## Conventional vs green technologies

### ➤ Scenario -1

- SMR to produce syngas followed by F-T synthesis

### ➤ Scenario-2

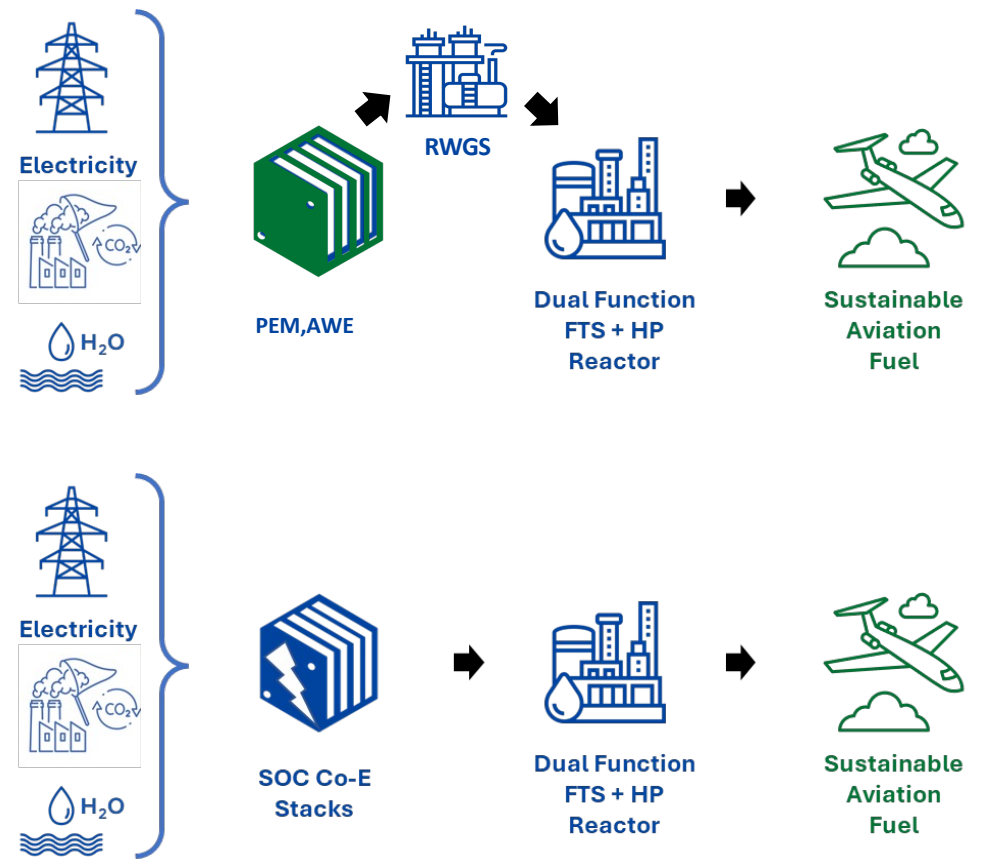
- Low temperature electrolysis followed by RWGS reactor and F-T synthesis

### ➤ Scenario-3

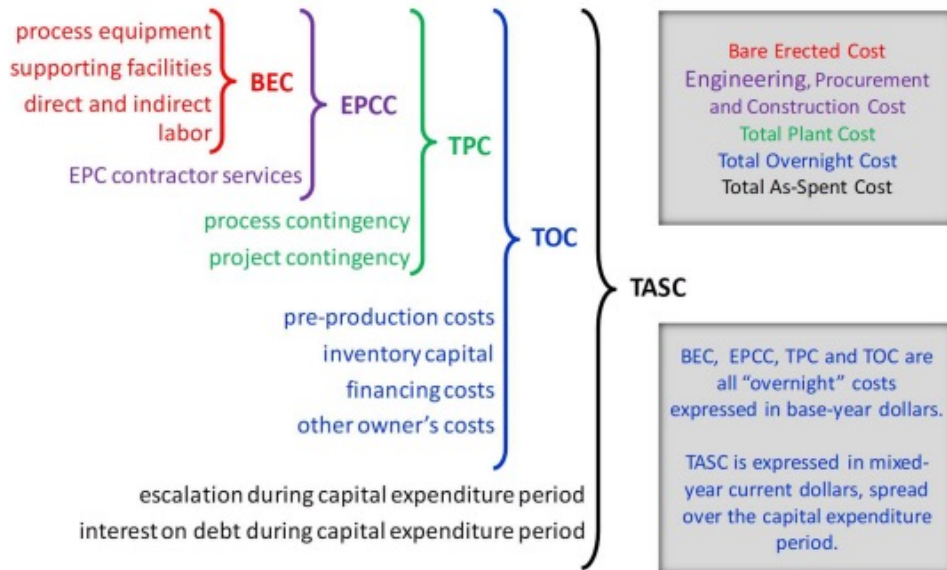
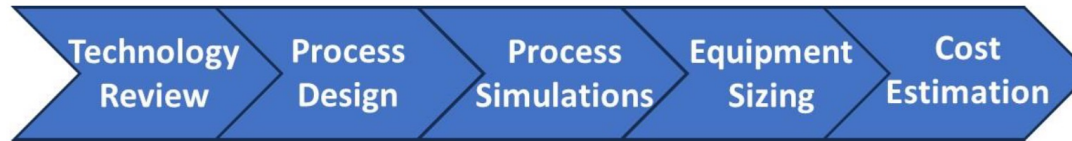
- High temperature co-electrolysis to produce syngas followed by F-T synthesis

### ➤ Assumptions

- Plant capacity 1kg/s (sensitivity 0.1-5kg/s)
- Electricity cost \$30/MWh (sensitivity \$25-90/MWh)
- Cost of stack is \$1000/kW (sensitivity \$250-2000/KW)
- Stack life is 10 years (sensitivity 5-20 years)
- Costs for CO<sub>2</sub> (\$40/ton), water (\$1.67/1000gallon)



# TEA Methodology and KPI's

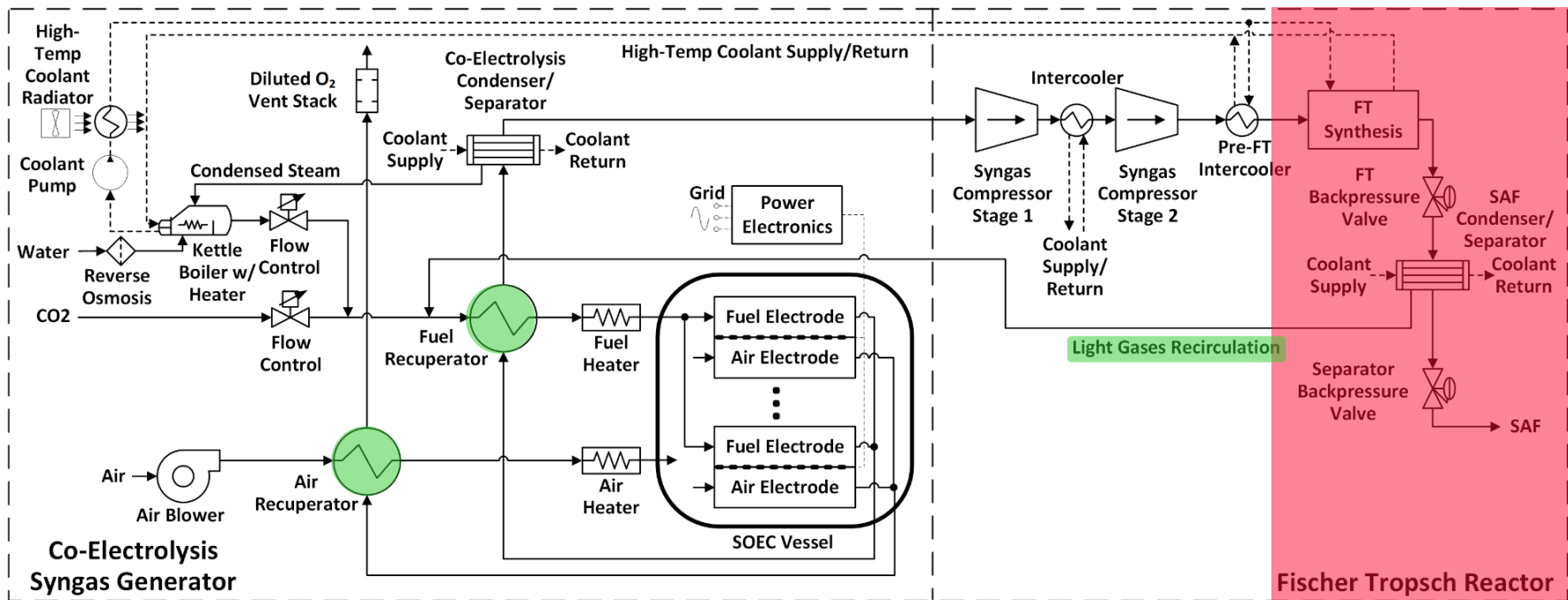


Key Performance Indicators	Values
Syngas Production Capacity (kg/s)	1.0
Electrolyzer Operating Conditions	750°C, 4 barg
Feed H <sub>2</sub> O Flow to SOEC (kg/s)	1.1
Feed CO <sub>2</sub> Flow to SOEC (kg/s)	1.5
Sweep Air Flow to SOEC (kg/s)	7.1
Single Pass Stack Conversion (%)	75%
Overall Conversion (%)	85%
Number of Cells per Stack	80
Number of Cells	160,000
SOEC Sweep/O <sub>2</sub> Outlet O <sub>2</sub> Content	≤ 35%
Syngas Quality for SAF Production	~ 20 barg, H <sub>2</sub> :CO = 2:1
F-T Liquid Production Capacity (bbl./day)	~ 180
SAF Production Capacity (bbl./day)	~ 60

$$LCOS = \frac{(FCR)(TASC) + OC_{FIX} + (CF)(OC_{VAR}) + CF(FC)}{(CF)(F_{SG})}$$

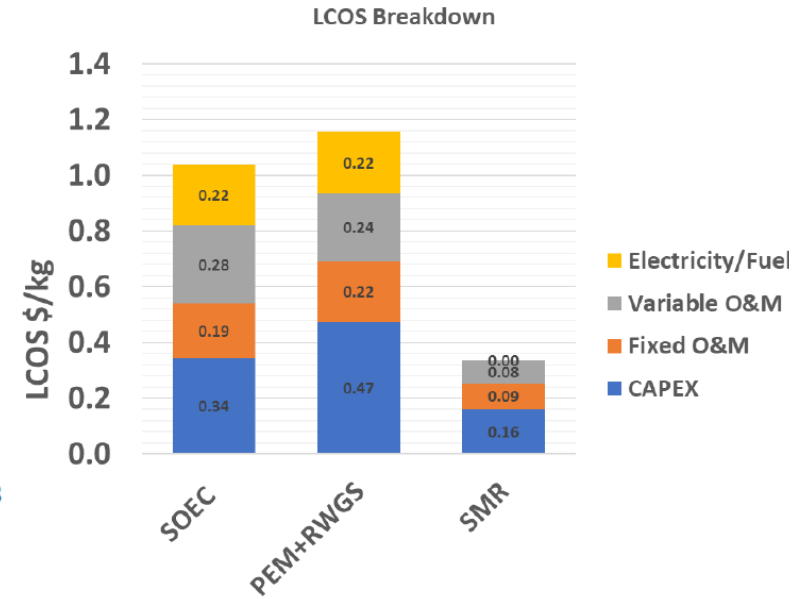
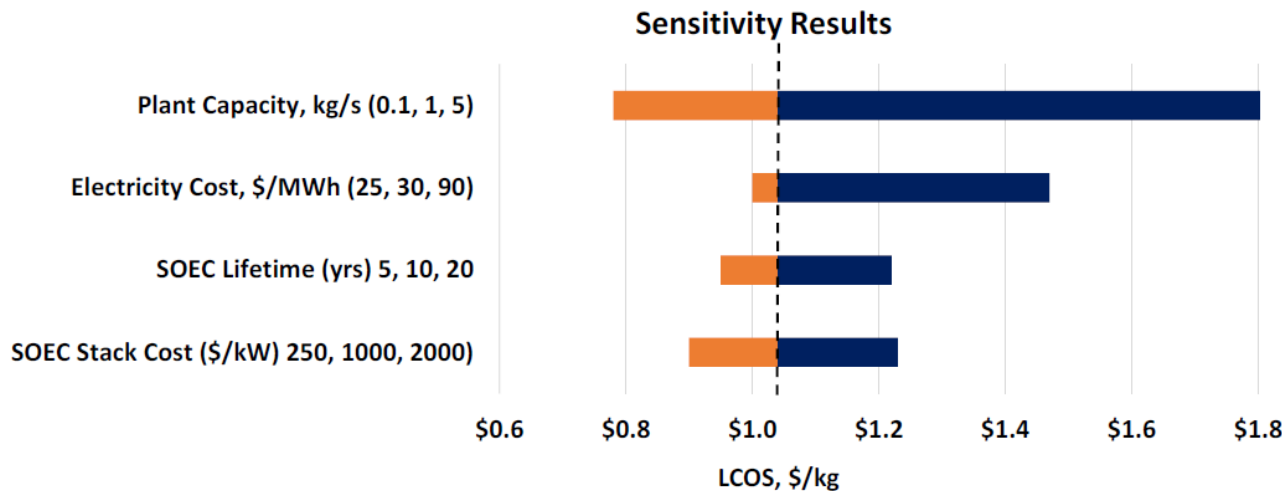
# Process flow diagram (PFD)

## TEA focus on syngas generation (not on conversion to SAF)





## Conventional vs Green technologies

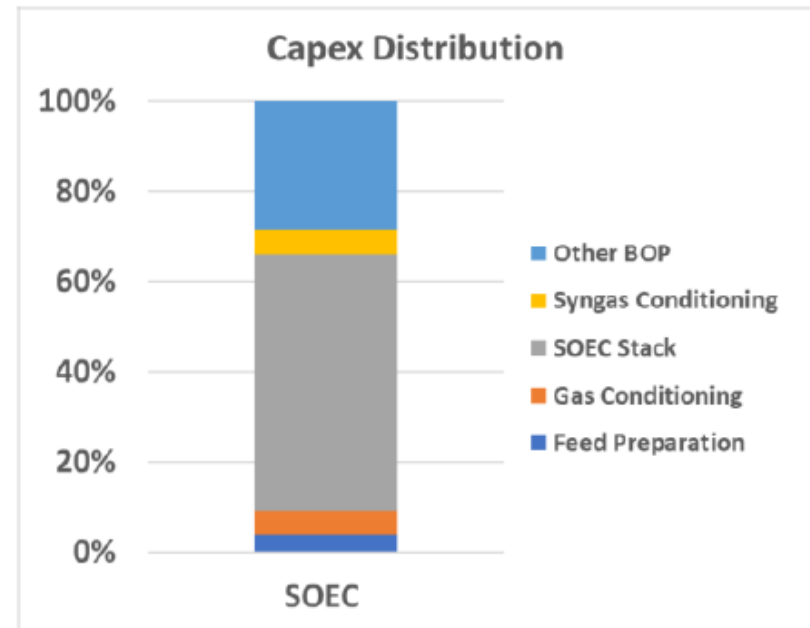


- Economies of scale is important for cost reduction
- Capex cost is the key differentiator for LT vs HT electrolysis (waste heat availability would advantage SOEC)



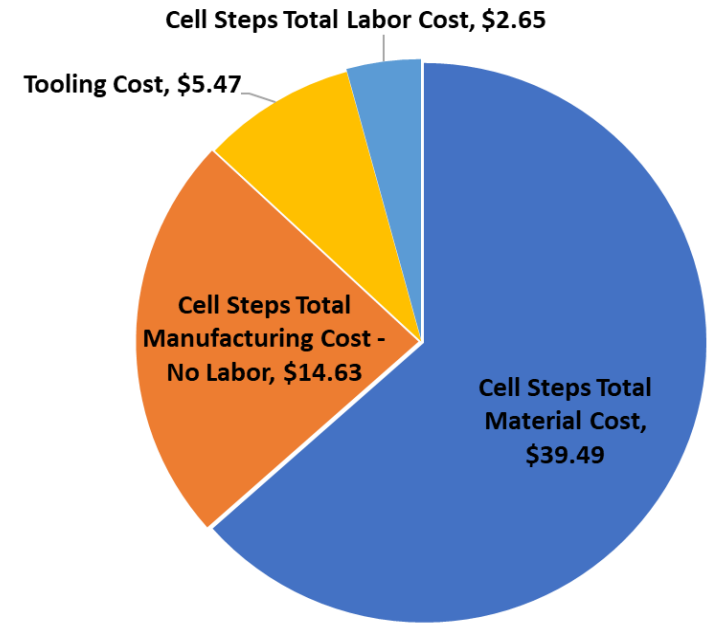
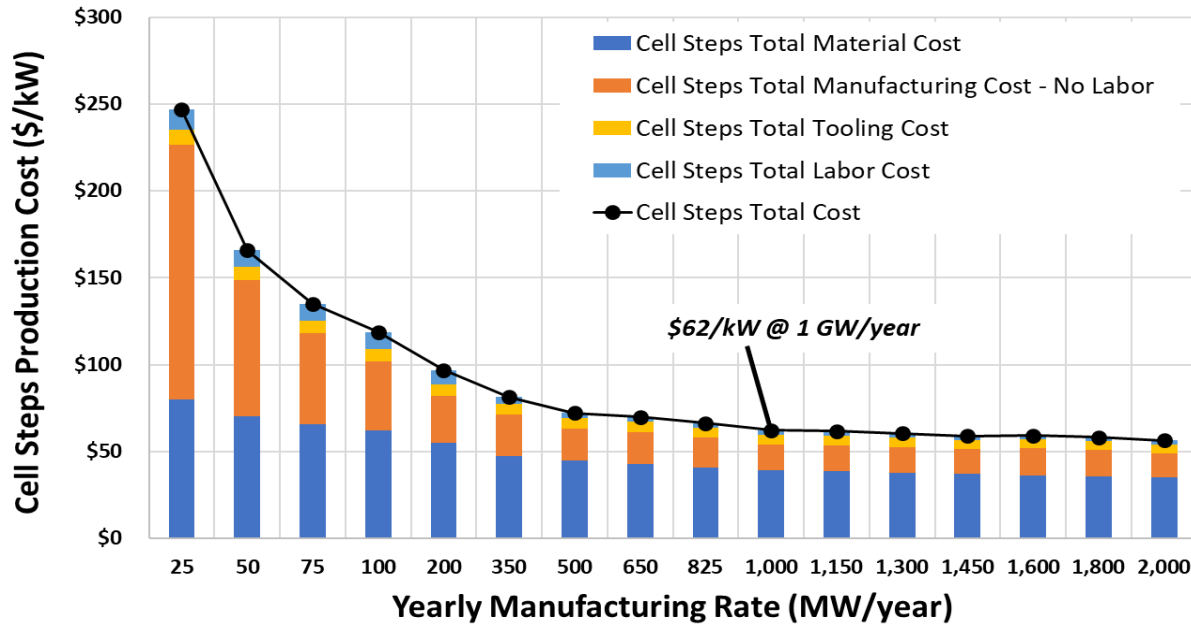
## Path for improvement by scale-up?

- Stack cost dominates the capex distribution
- Nexceris worked with a third party to identify pathway for cost reduction





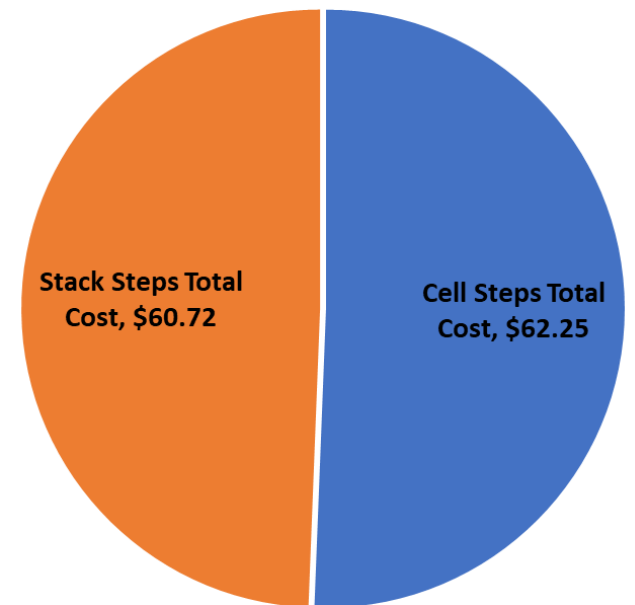
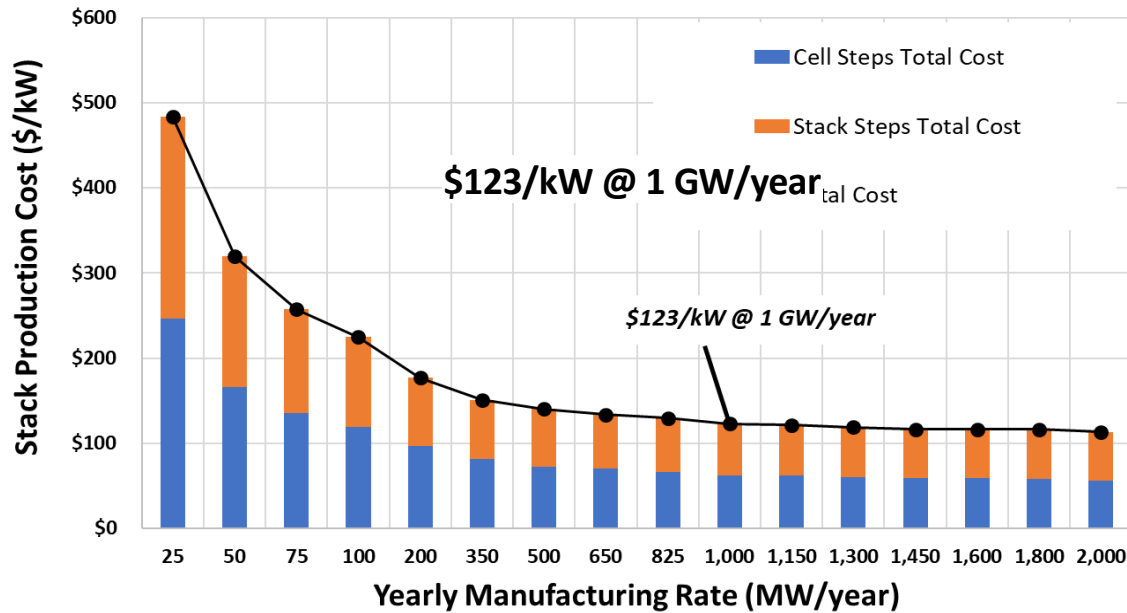
# Cost analysis for SOEC Cell Manufacturing



- Cost reduction opportunities around cell and stack materials as well as equipment utilization
- Bigger opportunities are volume, materials and process steps

## Stack cost at scale

- Total stack cost is \$122 per kW. Cell and stacking costs are essentially the same. The largest cost contributor to stacking is materials (53 percent).







## Future of Nexceris Solid Oxide Technologies

- Economies of scale is key to make it cost competitive compared to conventional technology
  - LCOS for Nexceris SOC is 10-15% better compared to LT technologies (room for further improvement)

### **What's next?**

- Recently signed \$60 million cost shared DOE cooperative agreement to scale up electrolysis stack technology to 20MW/year
- Long term durability and performance data on syngas production for accurate lifetime estimates
- Third-party evaluations of HTE stacks at INL and other partner sites.
- We look for strategic partners to scale up, demonstrate and commercialize our SOC technology.



## Nexceris Mission

Our vision is to create a better world through energy innovations.

We collaborate with leading global customers and partners to transform powerful ideas into solutions that make energy production safer, more efficient, and environmentally responsible.

**THANK YOU!**